



## VELOCITY VECTOR FIELD FOR FLUID FLOW

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### ABSTRACT

The description of a fluid flow requires a specification or determination of the velocity field, i.e. a specification of the fluid velocity at every point in the region. In general, this will define a vector field of position and time,  $\mathbf{u} = \mathbf{u}(x, t)$ . Steady flow occurs when  $\mathbf{u}$  is independent of time (i.e.,  $\partial\mathbf{u}/\partial t = 0$ ). Otherwise the flow is unsteady. Streamlines are lines which at a given instant are everywhere in the direction of the velocity (analogous to electric or magnetic field lines). In steady flow the streamlines are independent of time, but the velocity can vary in magnitude along a streamline (as in flow through a constriction in a pipe). Particle paths are lines traced out by “marked” particles as time evolves. In steady flow particle paths are identical to streamlines; in unsteady flow they are different, and sometimes very different. Particle paths are visualized in the laboratory using small floating particles of the same density as the fluid. Sometimes they are referred to as trajectories. Filament lines or streaklines are traced out over time by all particles passing through a given point; they may be visualized, for example, using a hypodermic needle and releasing a slow stream of dye. In steady flow these are streamlines; in unsteady flow they are neither streamlines nor particle paths. It should be emphasized that streamlines represent the velocity field at a specific constant of time, whereas particle paths and streaklines provide a representation of the velocity field over a finite period of time. In the laboratory we can obtain a record of streamlines photographically by seeding the fluid with small neutrally buoyant particles that move with the flow and taking a short exposure (e.g. 0.1 sec), long enough for each particle to trace out a short segment of line; the eye readily links these segments into continuous streamlines. Particle paths and streaklines are obtained from a time exposure long enough for the particle or dye trace to traverse the region of observation.

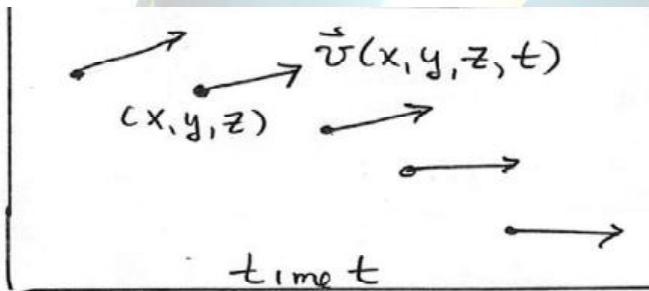
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### Introduction:

When we describe the flow of a fluid like water, we may think of the movement of individual particles. These particles interact with each other through

forces. We could then apply our laws of motion to each individual particle in the fluid but because the number of particles is very large, this would be an extremely difficult computation problem. Instead we shall begin by mathematically describing the state of moving fluid by specifying the velocity of the fluid at each point in space and at each instant in time.

For the moment we will choose Cartesian coordinates and refer to the coordinates of a point in space by the ordered triple  $(x, y, z)$  and the variable  $t$  to describe the instant in time, but in principle we may choose any appropriate coordinate system appropriate for describing the motion. The distribution of fluid velocities is described by the vector-valued function  $\vec{v}(x, y, z, t)$ . This represents the velocity of the fluid at the point  $(x, y, z)$  at the instant  $t$ . The quantity  $\vec{v}(x, y, z, t)$  is called the **velocity vector field**. It can be thought of at each instant in time as a collection of vectors, one for each point in space whose direction and magnitude describes the direction and magnitude of the velocity of the fluid at that point (Fig:1). This description of the velocity vector field of the fluid refers to fixed points in space and not to fixed moving particles in the fluid.



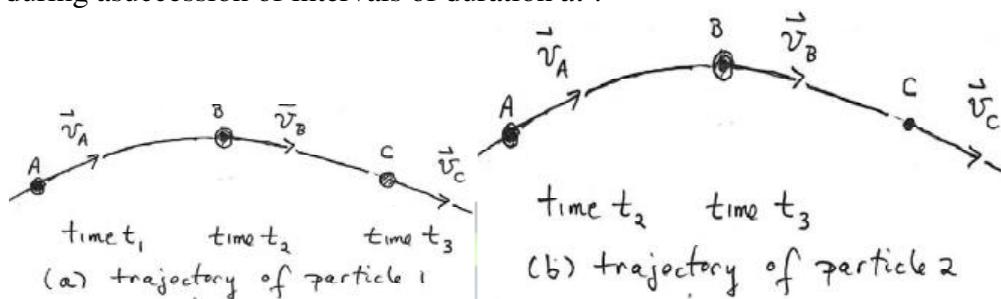
**Fig:1** Velocity vector field for fluid flow at time  $t$

We shall introduce functions for the pressure  $P(x, y, z, t)$  and the density  $\rho(x, y, z, t)$  of the fluid that describe the pressure and density of the fluid at each point in space and at Fig: 2 each instant in time. These functions are called **scalar fields** because there is only one number with appropriate units associated with each point in space at each instant in time. In order to describe the velocity vector field completely we need three functions  $v_x(x, y, z, t)$ ,  $v_y(x, y, z, t)$ , and  $v_z(x, y, z, t)$ .

For a non-ideal fluid, the differential equations satisfied by these velocity component functions are quite complicated and beyond the scope of this discussion. Instead, we shall primarily consider the special case of **steady flow** of a fluid in which the velocity

at each point in the fluid does not change in time. The velocities may still vary in space (non-uniform steady flow).

Let's trace the motion of particles in an ideal fluid undergoing steady flow during a succession of intervals of duration  $dt$ .



**Fig:2**(a) trajectory of particle 1, (b) trajectory of particle 2

Consider particle 1 located at point A with coordinates  $(x_A, y_A, z_A)$ . At the instant  $t_1$ , particle 1 will have velocity  $\mathbf{v}(x_A, y_A, z_A)$  and move to a point B with coordinates  $(x_B, y_B, z_B)$ , arriving there at the instant  $t_2 = t_1 + dt$ . During the next interval, particle 1 will move to point C arriving there at instant  $t_3 = t_2 + dt$ , where it has velocity  $\mathbf{v}(x_B, y_B, z_B)$  (Fig:2(a)). Because the flow has been assumed to be steady, at instant  $t_2$ , a different particle, particle 2, is now located at point A but it has the same velocity  $\mathbf{v}(x_A, y_A, z_A)$  particle 1 had at point A and hence will arrive at point B at the end of the next interval, at the instant  $t_3 = t_2 + dt$  (Fig:2(b)). In the third interval, particle 2, which began the interval at point B will end the interval at point C. In this way every particle has the same velocities at points along a streamline because we have not assumed that the velocity field is uniform. Particles that lie on the trajectory that our first particle traces out in time will follow the same trajectory. This trajectory is called a *streamline*. The particles in the fluid will not

**Mass Continuity Equation:** A set of streamlines for an ideal fluid undergoing steady flow in which there are no sources or sinks for the fluid is shown in Fig:3.

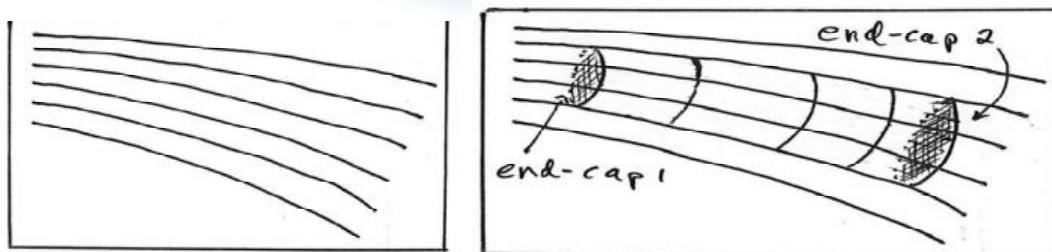




Fig:3 Set of streamlines for an ideal fluid flow Fig:4 Flux Tube associated with set of streamlines

We add to the flow tube two open surface (end-caps 1 and 2) that are perpendicular to velocity of the fluid, of areas  $A_1$  and  $A_2$  respectively. Because all fluid particles that enter end-cap 1 must follow their respective streamlines, they must all leave end-cap 2. If four streamlines that form the tube are sufficiently close together, we can assume that the velocity of the fluid in the vicinity of each end-cap surfaces is uniform.

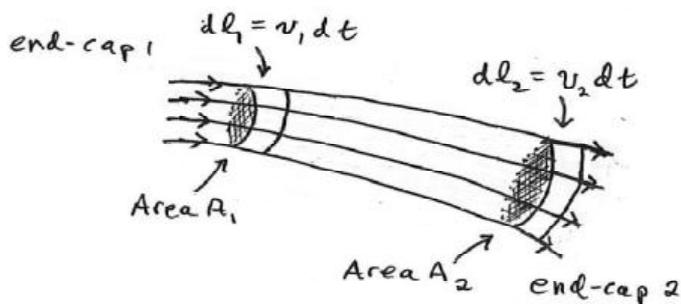


Fig: 5 Mass flow through flux tube

Let  $v_1$  denote the speed of the fluid near end-cap 1 and  $v_2$  denote the speed of the fluid near end-cap 2. Let  $\rho_1$  denote the density of the fluid near end-cap 1 and  $\rho_2$  denote the density of the fluid near end-cap 2. The amount of mass that enters and leaves the tube (Fig:4) in a time interval  $dt$  can be calculated as follows (Fig:5). Suppose we consider a small volume of space of cross-sectional area  $A_1$  and length  $dl_1 = v_1 dt$  near end-cap 1.

The mass that enters the tube in time interval  $dt$  is

$$dm_1 = \rho_1 dV_1 = \rho_1 A_1 dl_1 = \rho_1 A_1 v_1 dt \dots (1)$$

In a similar fashion, consider a small volume of space of cross-sectional area  $A_2$  and length  $dl_2 = v_2 dt$  near end-cap 2

The mass that leaves the tube in the time interval  $dt$  is then



$$dm_2 = \rho_2 dV_2 = \rho_2 A_2 dl_2 = \rho_2 A_2 v_2 dt \dots (2)$$

An equal amount of mass that enters end-cap 1 in the time interval  $dt$  must leave end-cap 2 in the same time interval, thus  $dm_1 = dm_2$ . Therefore using Eqs. (1) and (2),

$$\text{we have that } \rho_1 A_1 v_1 dt = \rho_2 A_2 v_2 dt .$$

Dividing through by  $dt$  implies that

$$\rho_1 A_1 v_1 = \rho_2 A_2 v_2 (\text{steady flow}) \dots (3)$$

Eq.(3) generalizes to any cross sectional area  $A$  of the thin tube, where the density is  $\rho$ , and the speed is  $v$ ,

$$\rho A v = \text{constant} (\text{steady flow}) \dots (4)$$

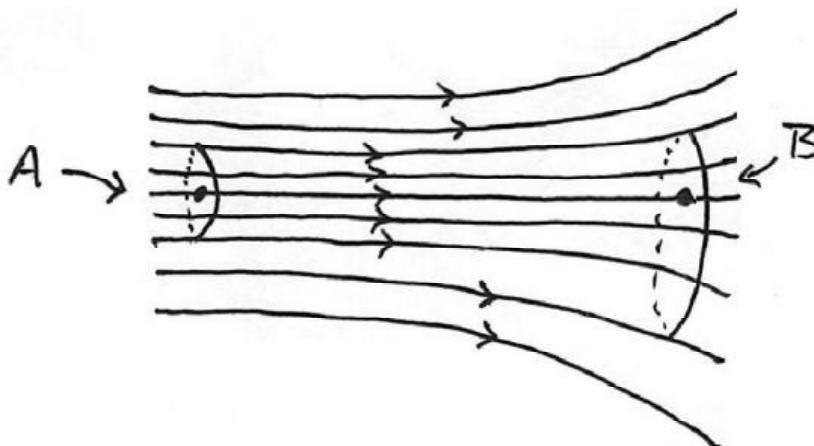
Eq. (3) is referred to as the *mass continuity equation for steady flow*. If we assume the fluid is incompressible, then Eq.(3) becomes

$$A_1 v_1 = A_2 v_2 (\text{incompressible fluid, steady flow}) \dots (5)$$

Consider the steady flow of an incompressible fluid with streamlines and closed surface formed by a streamline tube shown in Fig:5. According to Eq.(5), when the spacing of the streamlines increases, the speed of the fluid must decrease. Therefore the speed of the fluid is greater entering end-cap 1 than when it is leaving end-cap 2. When we represent fluid flow by streamlines, regions in which the streamlines are widely spaced have lower speeds than regions in which the streamlines are closely spaced.

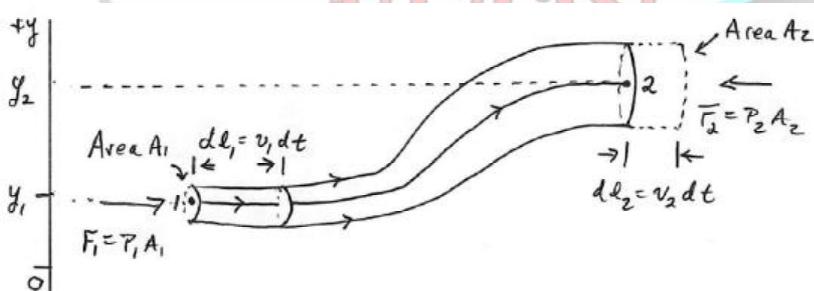
### **Bernoulli's Principle:**

Bernoulli's equation, one of the best-known and widely-used results of elementary fluid dynamics. Let's again consider the case of an ideal fluid that undergoes steady flow and apply energy methods to find an equation of state that relates pressure, density, and speed of the flow at different points in the fluid. Let's examine the case of a steady horizontal flow as seen in the overhead view shown in Fig: 6. We represent this flow by streamlines and a flow tube associated with the streamlines. Let's consider the motion of a fluid particle along one streamline passing through points  $A$  and  $B$  in Fig:6. The cross sectional area of the flow tube at point  $A$  is less than the cross-sectional area of the flow tube at point  $B$ .



**Fig:6** Overhead view of steady horizontal flow: in regions where spacing of the streamlines increases, the speed of the fluid must decrease.

According to Eq.(5), the particle located at point A has a greater speed than a fluid particle located at point B. Therefore a particle travelling along the streamline from point A to point B must decelerate. Because the streamline is horizontal, the force responsible is due to pressure differences in the fluid. Thus, for this steady horizontal flow in regions of lower speed there must be greater pressure than in regions of higher speed. Now suppose the steady flow of the ideal fluid is not horizontal, with the  $y$  – representing the vertical direction. The streamlines and flow tube for this steady flow are shown in Fig:7.



**Fig:7:** Non-horizontal steady flow

In order to determine the equation relating the pressure, speed and height difference of the tube, we shall use the work-energy theorem. We take as a system the mass contained in the flow tube shown in Fig:7. The external forces acting on our system are due to the pressure acting at the two ends of the flow tube and the



gravitational force. Consider a streamline passing through points 1 and 2 at opposite ends of the flow tube. Let's assume that the flow tube is narrow enough such that the velocity of the fluid is uniform on the cross-sectional areas of the tube at points 1 and 2. Point 1, denote the speed of a fluid particle by  $v_1$ , the cross-sectional area by  $A_1$ , the fluid pressure by  $P_1$  and the height of the centre of the cross-sectional area by  $y_1$ . At point 2, denote the speed of a fluid particle by  $v_2$ , the cross-sectional area by  $A_2$ , the fluid pressure by  $P_2$ , and the height of the centre of the cross-sectional area by  $y_2$ .

Consider the flow tube at time  $t$  as illustrated in Figure 28.7. At the left end of the flow, in a time interval  $dt$ , a particle at point 1 travels a distance  $dl_1 = v_1 dt$ . [5] proposed a principle in which another NN yield input control law was created for an under incited quad rotor UAV which uses the regular limitations of the under incited framework to create virtual control contributions to ensure the UAV tracks a craved direction. Utilizing the versatile back venturing method, every one of the six DOF are effectively followed utilizing just four control inputs while within the sight of un demonstrated flow and limited unsettling influences. Elements and speed vectors were thought to be inaccessible, along these lines a NN eyewitness was intended to recoup the limitless states. At that point, a novel NN virtual control structure which permitted the craved translational speeds to be controlled utilizing the pitch and the move of the UAV. At long last, a NN was used in the figuring of the real control inputs for the UAV dynamic framework. Utilizing Lyapunov systems, it was demonstrated that the estimation blunders of each NN, the spectator, Virtual controller, and the position, introduction, and speed following mistakes were all SGUUB while unwinding the partition Principle.

Therefore a small volume  $dV_1 = A_1 dl_1 = A_1 v_1 dt$  of fluid is displaced at the right end of the flow tube. In a similar fashion, a particle at point 2, travels a distance  $dl_2 = v_2 dt$ .

Therefore a small volume of fluid  $dV_2 = A_2 dl_2 = A_2 v_2 dt$  is also displaced to the right in the flow tube during the time interval  $dt$ . Because we are assuming the fluid is incompressible, by Eq.(5), these volume elements are equal,

$$dV = dV_1 = dV_2 .$$

There is a force of magnitude  $F_1 = P_1 A_1$  in the direction of the flow arising from the fluid pressure at the left end of the tube acting on the mass element that enters the tube. The work done displacing the mass element is then

$$dW_1 = F_1 dl_1 = P_1 A_1 dl_1 = P_1 dV \dots\dots 1$$



There is also a force of magnitude  $F_2 = P_2A_2$  in the direction opposing the flow arising from the fluid pressure at the right end of the tube. The work done opposing the displacement of the mass element leaving the tube is then

$$dW_1 = -F_2 dl_2 = -P_2 A_2 dl_2 = -P_2 dV \dots\dots 2$$

Therefore the external work done by the force associated with the fluid pressure is the sum of the work done at each end of the tube

$$dW^{ext} = dW_1 + dW_2 = (P_1 - P_2) dV \dots\dots 3$$

In a time interval  $dt$ , the work done by the gravitational force is equal to

$$dW^g = -dm g (y_2 - y_1) = -\rho dV g (y_2 - y_1) \dots\dots 4$$

Because we only chose the mass in the flow tube as our system, and we assumed that the fluid was ideal (no frictional losses due to viscosity) the change in the potential energy of the system is

$$dU = -W^g = \rho dV g (y_2 - y_1) \dots\dots 5$$

At time  $t$ , the kinetic energy of the system is the sum of the kinetic energy of the small mass element of volume  $dV = A_1 dl_1$  moving with speed  $v_1$  and the rest of the mass in the flow tube. At time  $t + dt$ , the kinetic energy of the system is the sum of the kinetic energy of the small mass element of volume  $dV = A_2 dl_2$  moving with speed  $v_2$  and the rest of the mass in the flow tube. The change in the kinetic energy of the system is due to the mass elements at the two ends and therefore

$$dK = 1/2 dm_2 v_2^2 - 1/2 dm_1 v_1^2 = 1/2 \rho dV (v_2^2 - v_1^2) \dots\dots 6$$

The work-energy theorem  $dW^{ext} = dU + dK$  for system is then

$$(P_1 - P_2) dV = 1/2 \rho dV (v_2^2 - v_1^2) + \rho g (y_2 - y_1) dV \dots\dots 7$$

We now divide Eq. (28.4.7) through by the volume  $dV$  and rearrange terms, yielding

$$P_1 + \rho g y_1 + 1/2 \rho v_1^2 = P_2 + \rho g y_2 + 1/2 \rho v_2^2 \dots\dots 8$$

Because points 1 and 2 were arbitrarily chosen, we can drop the subscripts and write Eq. (8) as

$$P + \rho g y + 1/2 \rho v^2 = \text{constant (ideal fluid, steady flow)} \dots\dots 9$$



Eq. (9) is known as **Bernoulli's Equation**.

Bernoulli's equation is one of the most important/useful equations in fluid mechanics. When the Bernoulli equation is combined with the continuity equation the two can be used to find velocities and pressures at points in the flow connected by a streamline.. The phenomenon that pressure decreases as velocity increases - sometimes comes in very useful in engineering. (It is on this principle that carburettor in many car engines work - Pressure reduces in a contraction allowing a small amount of fuel to enter).

**Conclusion:**

Streamlines are lines which at a given instant are everywhere in the direction of the velocity (analogous to electric or magnetic field lines). In steady flow the streamlines are independent of time, but the velocity can vary in magnitude along a streamline (as in flow through a constriction in a pipe). It should be emphasized that streamlines represent the velocity field at a specific constant of time, whereas particle paths and streaklines provide a representation of the velocity field over a finite period of time.

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